

# Conduction

• Remember :-  $\dot{q}_x = \frac{\dot{q}_x}{A} = -K \frac{dT}{dx}$  (1)

An alternative form of (1) is:-

$$\boxed{\dot{q}_x = \frac{\dot{q}_x}{A} = -K \frac{\partial T}{\partial x}}$$

Partial diff. → T distribution  
 Depends on x & t so we use ∂

## The Heat Diffusion Equation

Recall energy conservation

$$\dot{E}_{in} + \dot{E}_g - \dot{E}_{out} = \dot{E}_{st}$$

For x :-  $\dot{q}_x + \dot{q} dx - \dot{q}_{x+dx} = \rho c_p \frac{\partial T}{\partial t} dx$  (2)

Given  $\rightarrow \dot{q}_x - \dot{q}_{x+dx} = \frac{\partial}{\partial x} \left( K \frac{\partial T}{\partial x} \right) dx$

So (2) Becomes:-

$$\frac{\partial}{\partial x} \left( K \frac{\partial T}{\partial x} \right) dx + \dot{q} dx = \rho c_p \frac{\partial T}{\partial t} dx$$

$$\frac{\partial}{\partial x} \left( K \frac{\partial T}{\partial x} \right) + \dot{q} = \underbrace{\rho c_p \frac{\partial T}{\partial t}}_{\text{can be replaced by } \frac{K}{\alpha}}$$

can be replaced by  $\frac{K}{\alpha}$

[2]

## Special cases

[1] Steady-state conditions:  $\rho c_p \frac{\partial T}{\partial t} = 0$

↳ So Diffusion equation becomes

$$\dot{q} = - \frac{\partial}{\partial x} \left( k \frac{\partial T}{\partial x} \right)$$

[2] No energy generation:  $\dot{q} = 0$

↳ So Diffusion equation becomes

$$\frac{\partial}{\partial x} \left( k \frac{\partial T}{\partial x} \right) = \rho c_p \frac{\partial T}{\partial t}$$

If we are using other coordinates :-

Cylindrical :-

3-Directions

$$\frac{1}{r} \frac{\partial}{\partial r} \left( k r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial}{\partial \phi} \left( k \frac{\partial T}{\partial \phi} \right) + \frac{\partial}{\partial z} \left( k \frac{\partial T}{\partial z} \right) + \dot{q} = \rho c_p \frac{\partial T}{\partial t}$$

Spherical:  
3-Directions

$$\frac{1}{r^2} \frac{\partial}{\partial r} \left( k r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial}{\partial \phi} \left( k \frac{\partial T}{\partial \phi} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( k \sin \theta \frac{\partial T}{\partial \theta} \right) + \dot{q} = \rho c_p \frac{\partial T}{\partial t}$$

# Boundary Conditions

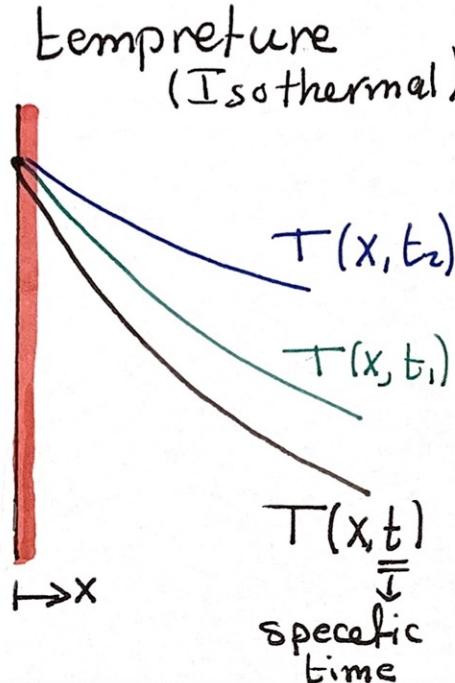
at  $x=0$

## 1. Constant surface temperature (Isothermal)

- at  $x=0$ , at  $T_s$  any time

$$\text{const.} \rightarrow T_s = T(x=0, t)$$

مكانتها اتومعند طبع  
اکرارة سبادی  
اوی زمن



## 2.a: Constant surface heat flux

→ Finite heat flux

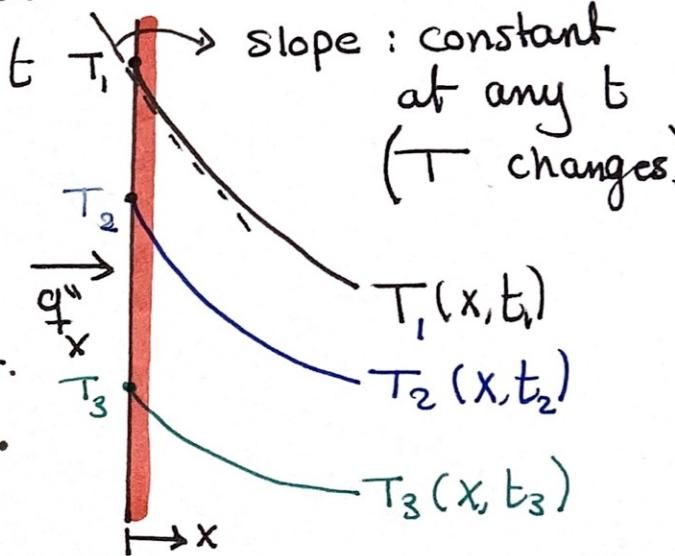
- at  $x=0$ , at any  $t$   $T_s$

$q''_x$  is constant

$$q''_x = -k \left. \frac{\partial T}{\partial x} \right|_{x=0}$$

Slope of tangent: const.

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اوی زمن  
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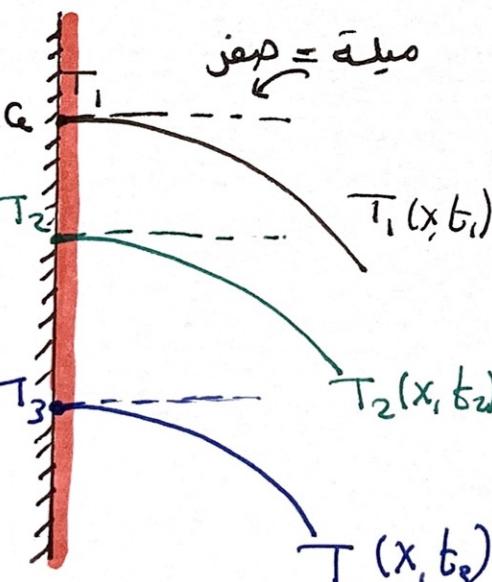


## 2.b: Constant Surface heat flux

→ Adiabatic or insulated surface

$$q''_x = 0 = \left. \frac{\partial T}{\partial x} \right|_{x=0}$$

مكانتها اتومعند اوی زمان او  
اوی زمان دفعه حرارة او  
اوی زمان دفعه حرارة او



## 3. Convection surface condition

$$-k \left. \left( \frac{\partial T}{\partial x} \right) \right|_{x=0} = h [T_\infty - T(0, t)]$$

مكانتها اتومعندی او  
اوی زمان دفعه الحرارة او  
اوی زمان دفعه الحرارة او

convective  
heat transfer  
conditions

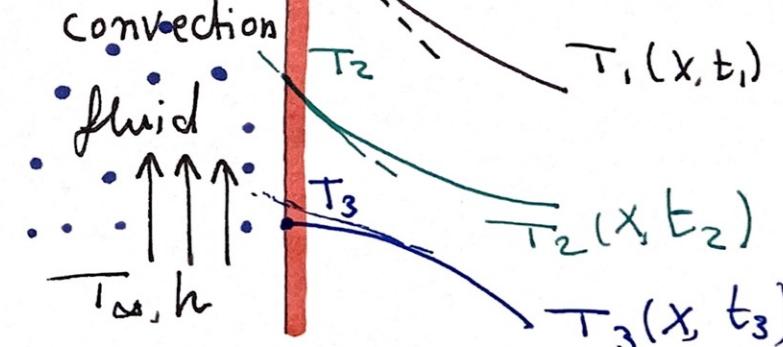
convection

fluid

...

$T_\infty, h$

Note:  
 $T_\infty > T_0$   
 $q_{\text{conv}} = q_{\text{cond}} \cdot T_\infty < T$



## Thermal conductivity: (K)

$$K_{\text{solids}} \gg K_{\text{liquid}} \gg K_{\text{gas}}$$

• In Solids:-

$$K = K_e + K_L$$

free electron                      lattice vibration

→ For Pure metals:-

$$K_e = L_o T / \rho_e \rightarrow \text{electrical resistivity}$$

↓    Lorenz number

→ non metallic solids:-

$$K \rightarrow \text{due to } K_L$$

Thermal diffusivity  $\alpha$

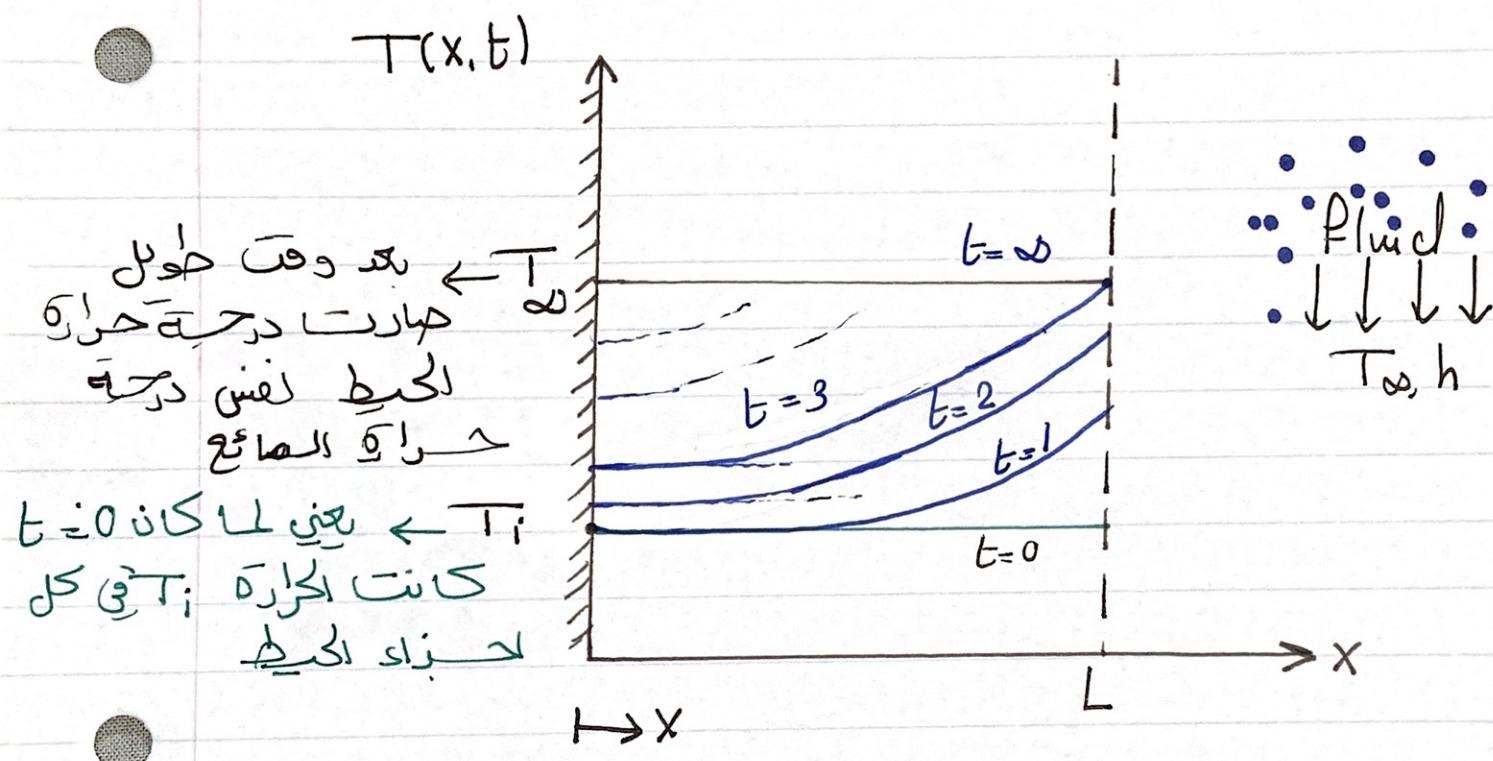
$$\alpha = \frac{k}{\rho c_p}$$

$\alpha_{\text{metals}} > \alpha_{\text{non metals}}$

## Explaining $T(x, t)$ , X curves

$T(x, t)$ : Distribution of temperature

- Usually it is required to draw  $T(x, t)$  vs  $X$  curve for conditions :- initial :  $t \leq 0$
- Take Q 2.57 as an example steady-state :  $t \rightarrow \infty$   
two intermediate times



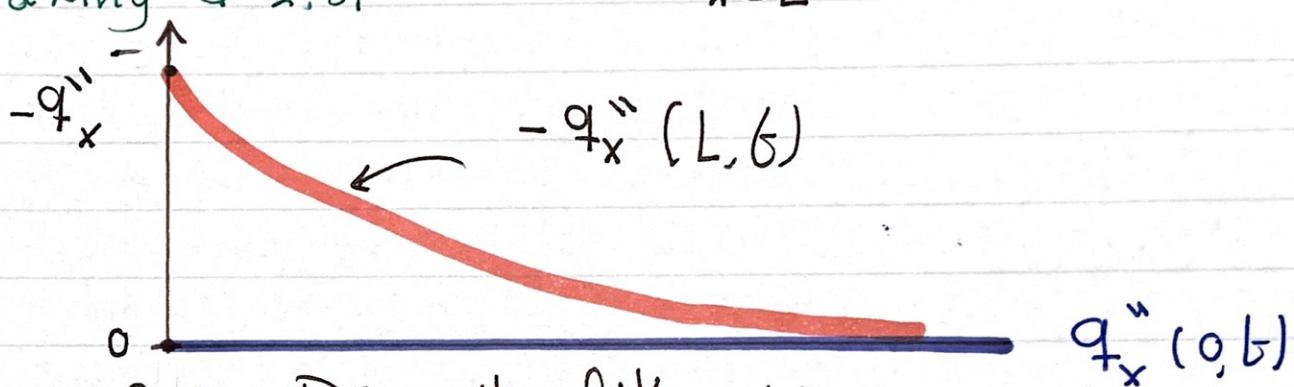
- Initially,  $T = T_i$
- Suddenly,  $x=L$  is heated
- lastly, It reached to a state in which  $T_L = T_\infty$

Notice : at  $x=0$  Insulation  $\rightarrow$   $x=0$  لا ينبع حرارة صفر

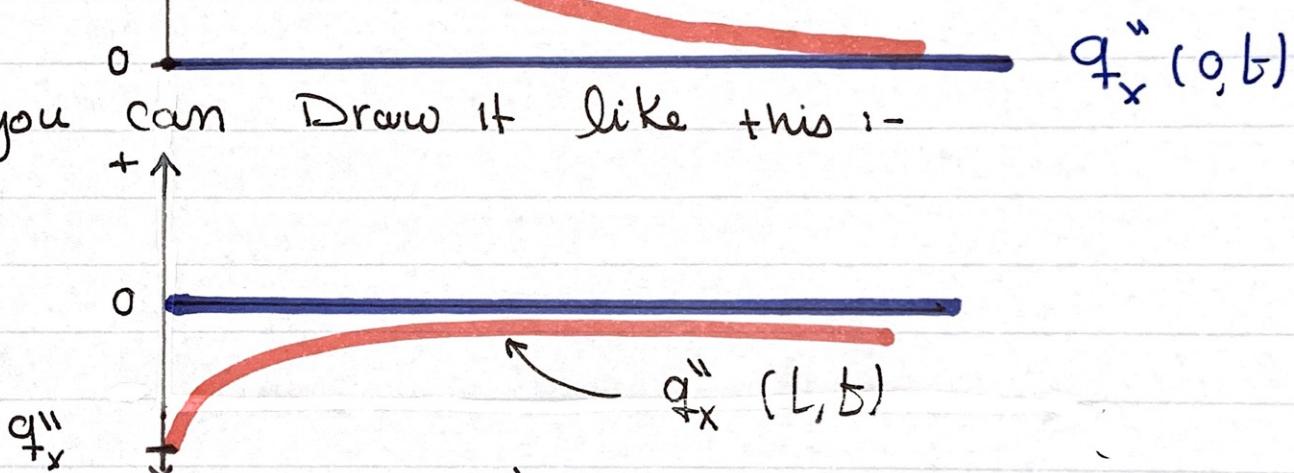
## Explaining $q''_x(x,t)$ vs $t$ curves

$q''_x$  : Flux distribution

- Usually it is required to draw  $q''_x(x,t)$  vs  $t$  curve for conditions :-  $x=0$
- Taking  $\textcircled{1} 2.5f$   $x=L$



or you can draw it like this :-



- \* First: taking  $q''_x(0,t)$  : at  $x=0$ , insulated so  $q''=0$  with time  $T$  is const. because of the insulation

- \* Second: taking  $q''_x(L,t)$  : at  $x=L$ , it is heated so it gains heat, it starts at a max value (heat it gained from fluid) and decreases until it reaches zero when  $T_L = T_\infty$